Amendments to the Claims:

1. (Currently Amended) A process for the preparation of a gas containing hydrogen and carbon monoxide from a carbonaceous feedstock, the process comprising:

(a) partially oxidizing a carbonaceous feedstock in a vertically oriented tubular partial oxidation reactor vessel having an upper end, and a lower end having an inlet, the vessel comprising a burner at the upper end thereby obtaining a first gaseous product of hydrogen and carbon monoxide having a temperature between 1100 °C and 1500 °C;

(b) catalytically steam reforming a carbonaceous feedstock in the presence of steam in a convective steam reformer zone in a second vessel thereby obtaining a steam reformer product;

(c) reducing the temperature of the first gaseous product by between 300 °C and 750 °C by mixing the first gaseous product with the steam reformer product by feeding the steam reformer product into ~~the~~ said inlet yielding a first mixture;

(d) contacting the first mixture with a bed of reforming catalyst positioned in the lower end of the partial oxidation reactor vessel just below ~~the~~ said inlet and obtaining a second mixture having a temperature between 950 °C and 1100 °C; and

(e) feeding the second mixture to the second vessel and providing heat for the convective steam reforming reaction zone in step (b) by convective heat exchange between the second mixture having a temperature between 950 °C and 1100 °C and the steam reformer reactor zone thereby obtaining a hydrogen and carbon monoxide containing gas having a reduced temperature.

2. (Previously Presented) The process of claim 1, wherein the steam to carbon molar ratio of the feed to step (b) is between 0.5 and 0.9.

3. Canceled.

4. (Previously Presented) The process of claim 1, wherein the content of methane in the steam reformer product is between 1 mol% and 10 mol% relative to the carbon present as hydrocarbon in the carbonaceous feed to step (b).

5. (Previously Presented) The process of claim 1, wherein the methane conversion in step (d) is between 10 wt% and 50 wt%.

6. (Previously Presented) The process of claim 1, wherein the temperature of the mixture obtained in step (d) is between 980 °C and 1050 °C.
